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(54) SYSTEM AND METHOD FOR GENERATING **PARTICLES**

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- U.S. Cl. USPC 205/220; 205/102; 205/265; 205/627
- Field of Classification Search 204/229.4, 204/660, 663; 205/339, 340, 565, 627, 102, 205/220, 265, 441

See application file for complete search history.

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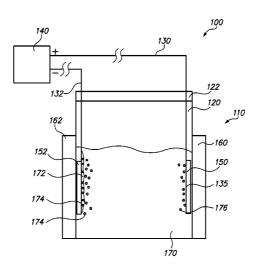
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(57)ABSTRACT

A method may include the steps of supplying current to the electrodes of an electrochemical cell according to a first charging profile, wherein the electrochemical cell has an anode, cathode, and electrolytic solution; maintaining a generally constant current between the electrodes; exposing the cell to an external field either during or after the termination of the deposition of deuterium absorbing metal on the cathode; and supplying current to the electrodes according to a second charging profile during the exposure of the cell to the external field. The electrolytic solution may include a metallic salt including palladium, and a supporting electrolyte, each dissolved in heavy water. The cathode may comprise a second metal that does not substantially absorb deuterium, such as gold. The external field may be a magnetic field.

7 Claims, 10 Drawing Sheets



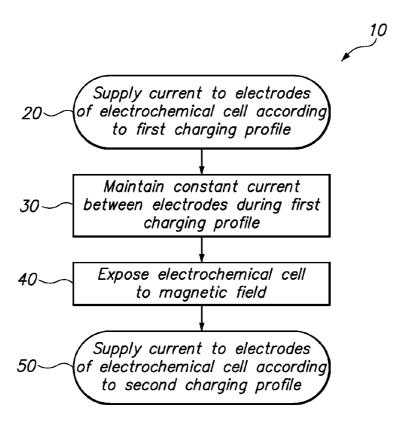
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Supply a current of 100µA to electrodes for 24 hours

Supply a current of 200µA to electrodes for 48 hours

Supply a current of 500µA to electrodes until deposition completion

FIG. 2

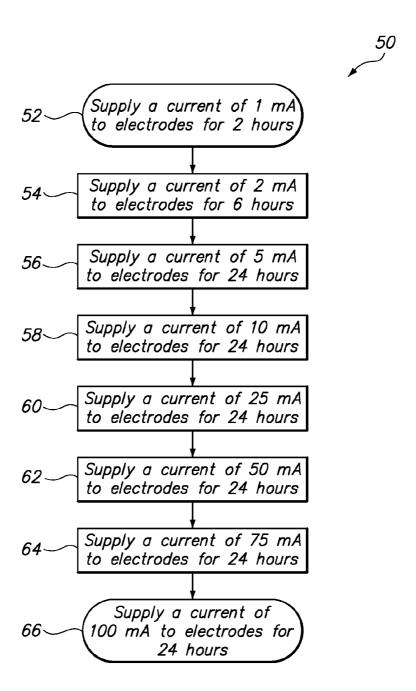


FIG. 3

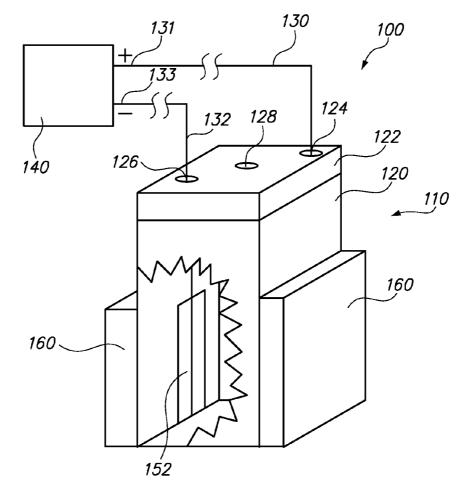


FIG. 4

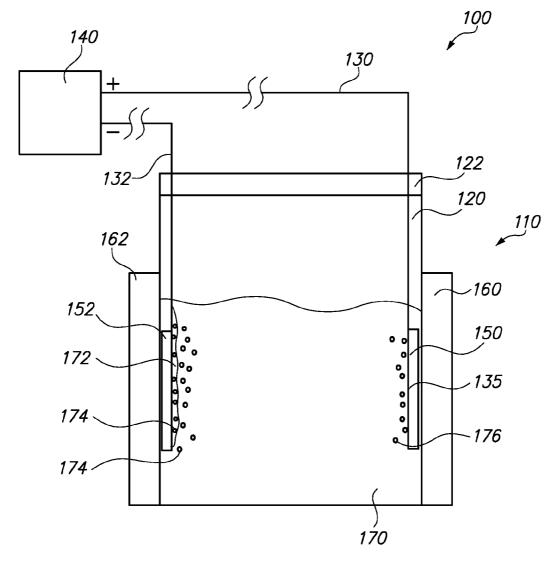
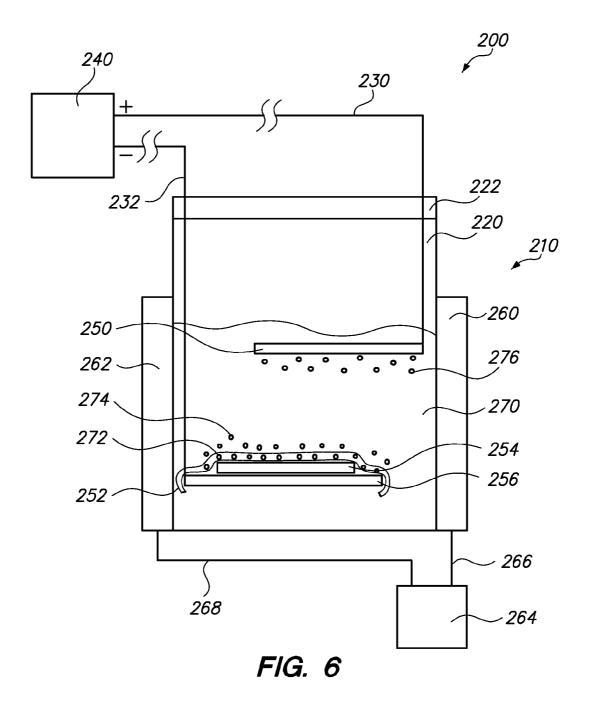
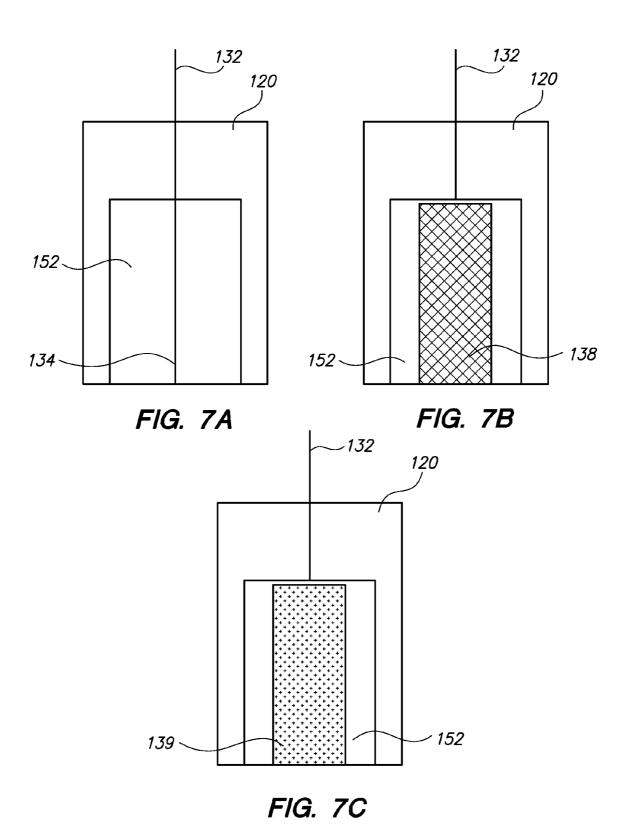


FIG. 5





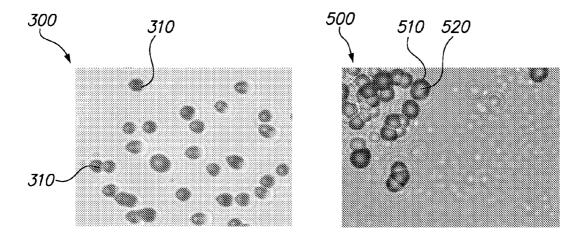


FIG. 8A

FIG. 8C

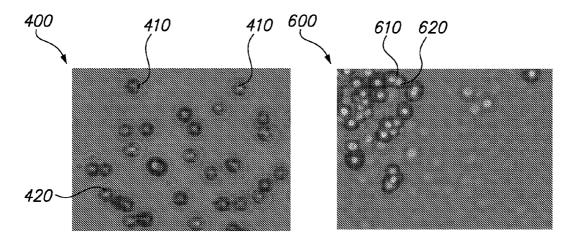


FIG. 8B

FIG. 8D

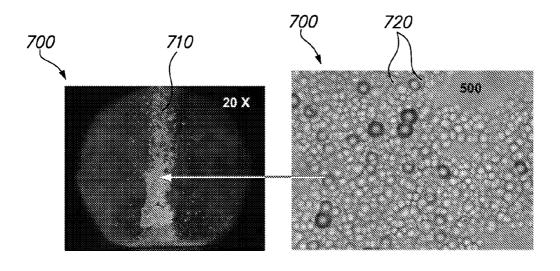


FIG. 9A

FIG. 9B

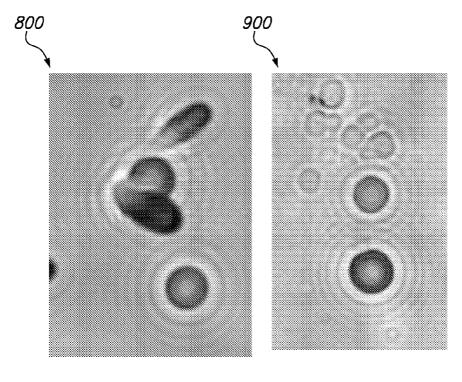


FIG. 10A

FIG. 10B

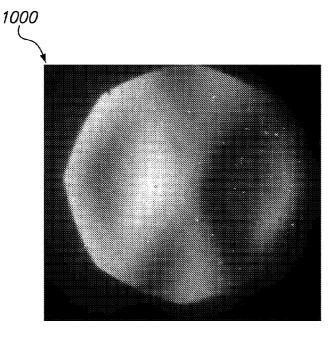
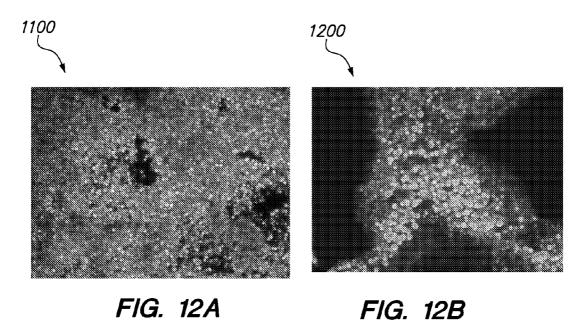


FIG. 11



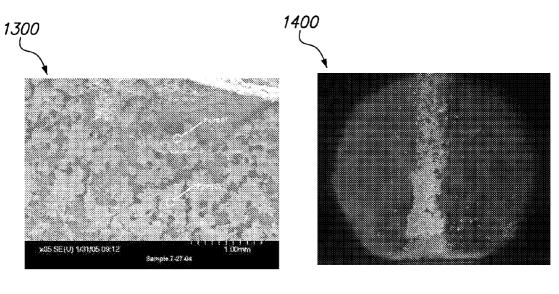


FIG. 13A FIG. 13B

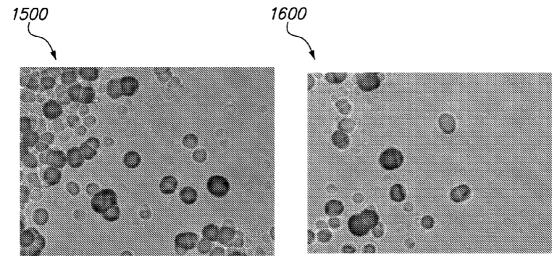


FIG. 13C

FIG. 13D

SYSTEM AND METHOD FOR GENERATING **PARTICLES**

CROSS-REFERENCE TO RELATED APPLICATIONS

This application claims the benefit of U.S. Provisional Patent Application Ser. No. 60/919,190, filed Mar. 14, 2007, entitled "Method and Apparatus for Generating Particles," the content of which is fully incorporated by reference herein.

BACKGROUND OF THE INVENTION

The embodiments of the invention relate generally to the field of electrochemistry.

Generated particles may be captured by other nuclei to create new elements, to remediate nuclear waste, to treat cancerous tumors, or to create strategic materials. Previous efforts to create a reproducible method and corresponding in heavy water have been unsuccessful.

Therefore, a need currently exists for a reproducible method and corresponding system that can generate particles.

BRIEF DESCRIPTION OF THE DRAWINGS

- FIG. 1 illustrates a flow chart of an implementation of a method for generating particles.
- FIG. 2 illustrates a flow chart of an implementation of a first charging profile for an implementation of the method for 30 generating particles.
- FIG. 3 illustrates a flow chart of an implementation of a second charging profile for an implementation of the method for generating particles.
- FIG. 4 illustrates a front perspective view of an embodi- 35 ment of a system for generating particles using an external magnetic field.
- FIG. 5 illustrates a cross-section view of an embodiment of a system for generating particles using an external magnetic field, during a co-deposition process.
- FIG. 6 illustrates a cross-section view of an embodiment of a system for generating particles using an external electric field
- FIG. 7A illustrates a front view of one side of an embodiment of a system for generating particles using an external 45 magnetic field, illustrating an embodiment of the cathode.
- FIG. 7B illustrates a front view of one side of an embodiment of a system for generating particles using an external magnetic field, illustrating an embodiment of the cathode.
- FIG. 7C illustrates a front view of one side of an embodiment of a system for generating particles using an external magnetic field, illustrating an embodiment of the cathode.
- FIGS. 8A and 8B show images of alpha particle tracks in a CR-39 detector, where the microscope optics are focused on the surface of the detector and the bottom of the pits, respec- 55 tively.
- FIGS. 8C and 8D show images of Pd/D co-deposition generated tracks in a CR-39 detector, where the microscope optics are focused on the surface of the detector and the bottom of the pits, respectively.
- FIGS. 9A and 9B show images taken of the CR-39 detector after a Pd/D co-deposition experiment in a magnetic field.
- FIG. 10A shows features observed when a CR-39 detector is exposed to depleted Uranium.
- FIG. 10B shows features observed when a CR-39 detector 65 has undergone exposure to a Pd/D co-deposition experiment in the presence of an external electric field.

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- FIG. 11 illustrates an image of a CR-39 detector indicating X-ray emission, in accordance with an embodiment of the system and method for generating particles.
- FIG. 12A shows an image taken of a CR-39 detector after a Pd/D co-deposition experiment on a Ni screen cathode in the presence of a magnetic field.
- FIG. 12B shows an image of a CR-39 detector after a Pd/D co-deposition experiment on a Ni/Au composite cathode in which Au is a high Z material.
- FIG. 13A shows an SEM of the Pd deposit obtained on a Au foil cathode in a magnetic field experiment.
- FIGS. 13B-13D show images taken of a CR-39 detector after a Pd/D co-deposition experiment in a magnetic field using a Ag wire cathode.

DETAILED DESCRIPTION OF SOME **EMBODIMENTS**

FIG. 1 shows a flow chart of an implementation of a system to generate particles during electrolysis of palladium 20 method for generating particles 10. One implementation of method 10 may utilize an electrochemical cell 100 as shown in FIGS. 4 and 5. As such, method 10 will be discussed with reference to electrochemical cell 100. Method 10 may be performed at conditions of ambient temperature and standard 25 atmospheric pressure. Method 10 may begin at step 20, where a current may be supplied to the electrodes of an electrochemical cell according to a first charging profile. For example, step 20 may involve supplying current to the positive electrode, anode 130, and the negative electrode, cathode 132, of electrochemical cell 100. Current may be supplied to anode 130 and cathode 132 by connecting a galvanostat/ potentiostat 140 to anode 130 and cathode 132. Step 20 is discussed in further detail with regard to FIG. 2. Following step 20, method 10 may proceed to step 30. Step 30 may involve maintaining a generally constant current between the positive and negative electrodes during the first charging profile such that deposition of metal 172 on the cathode occurs in the presence of evolving deuterium gas during electrolysis of an electrolytic solution. As an example, step 30 may involve maintaining a generally constant current between the anode 130 and cathode 132 during the first charging profile. Maintaining a generally constant current serves to ensure that deposition of metal 172 that substantially absorbs deuterium on cathode 132 occurs in the presence of evolving deuterium gas 174 during electrolysis of electrolytic solution 170 (see FIG. 5). A generally constant current may be defined as current that is stable, but that may have minor fluctuations. Step 30 may be performed by connecting a galvanostat/potentiostat 140 to anode 130 and cathode 132.

Method 10 may next proceed to step 40, where electrochemical cell 100 may be exposed to an external field, such as a magnetic field. For example, step 40 may be performed by positioning magnets 160 and 162 opposite one another on opposing sides of electrochemical cell 100 (see FIGS. 4 and 5). Step 40 may occur during the deposition of the metal on the cathode. In other embodiments, step 40 may occur after the termination of the deposition of the metal on the cathode. The determination that the deposition of the metal on the cathode has terminated may be made by a visual inspection that the plating solution within electrolytic solution 170 has turned from a red-brown color to clear. The plating solution turns clear when metal has all been plated onto cathode 132. Method 10 may then proceed to step 50, where a current may be supplied to the electrodes according to a second charging profile during the exposure of the electrochemical cell to the external field. For example, step 50 may involve using a power source to supply a current to anode 130 and cathode

132 according to a second charging profile during the exposure of electrochemical cell 100 to an external magnetic field (not shown).

Particles are generated from the application of method 10. As used herein, the term "generated" is used to refer to the 5 forming of particles through a process involving chemical and, depending upon the substrate, magnetic interaction. Examples of the types of particles generated and detected may include, but are not limited to: alpha particles, beta particles, gamma rays, energetic protons, deuterons, tritons, and neutrons. The particles generated by the implementations of method 10 may have various applications. For example, the generated particles may be captured by other nuclei to create new elements, may be used to remediate nuclear waste, may be used to create strategic materials, or may be used to treat 15 cancerous tumors. As an example there are some sites that have groundwater that is contaminated with radionuclides, such as technetium, Tc-99. The particles emitted by electrochemical cell 100 may be absorbed by the radionuclide, Tc-99 via neutron capture, transmuting it to Tc-100 with a 20 half life of 15.8 seconds to Ru-100, which is stable where the reaction is shown by $^{99}\text{Tc}_{43}(n,\gamma)^{100}\text{Tc}_{43}$ and the $^{100}\text{Tc}_{43}$ $\beta^$ decays to ¹⁰⁰Ru₄₄ with a half-life of 15.8 seconds.

FIG. 2 shows a flow chart of an implementation of step 20 of method 10. Step 20 may include more than one current 25 level and more than one time period, wherein each of the current levels is supplied across the anode and the cathode for one of the time periods. Step 20 may be performed to assure good adherence of the palladium, a deuterium absorbing metal, to cathode 132, which may be a wire having a length of 30 2 cm and a diameter of 0.5 cm. Step 20 may involve low current densities for adhering the palladium to cathode 132. As an example, step 20 may begin at step 22, where a reducing current of 100 µA may be supplied to the anode and cathode for a time period of about twenty-four hours. Next, step 24 35 may involve supplying a reducing current of 200 μA to anode 130 and cathode 132 for a time period of about forty-eight hours. Step 20 may then proceed to step 26, where a reducing current of 500 µA may be supplied to anode 130 and cathode 132 until the completion of the deposition process. The 40 completion of the deposition process will occur when the plating solution appears clear as described above. As an example, the amount of time required for the completion of the deposition process may be between approximately 3 and 7 days, depending upon the surface area of cathode 132 and 45 the first charging profile used.

As current is applied, Pd is deposited on the cathode. Electrochemical reactions occurring at the cathode include:

$$Pd^{2+}+2e^{-}Pd^{0}$$

$$D_2O + e^-D^0 \pm OD^-$$
 (Eq. 1)

Once formed, the D^0 is either absorbed by the Pd or binds to another D^0 to form a deuterium molecule, D_2 . At standard temperature and pressure, D_2 is a gas. The result is that metallic Pd is deposited on the cathode in the presence of evolving D_2 .

FIG. 3 illustrates a flow chart of an implementation of step 50 of method 10. Step 50 may be performed to load metal 172 on cathode 132 with deuterium. In one embodiment, step 50 may involve more than one current levels and more than one time periods, wherein each of the current levels is supplied across the anode and the cathode for one of the time periods. In one embodiment, step 50 may involve levels of increasing current density to load the palladium lattice with deuterium such that the ratio of deuterium to palladium is $\geqq 1$. As an example, one implementation of step 50 may begin at step 52,

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where a current of 1 mA is supplied to anode 130 and cathode 132 for a time period of about two hours. Next, step 54 may involve supplying a current of 2 mA to anode 130 and cathode 132 for a time period of about six hours. Next, step 56 may involve supplying a current of 5 mA to anode 130 and cathode 132 for a time period of about twenty-four hours. Next, step 58 may involve supplying a current of 10 mA to anode 130 and cathode 132 for a time period of about twenty-four hours. Next, step 60 may involve supplying a current of 25 mA to anode 130 and cathode 132 for a time period of about twentyfour hours. Next, step 62 may involve supplying a current of 50 mA to anode 130 and cathode 132 for a time period of about twenty-four hours. Next, step 64 may involve supplying a current of 75 mA to anode 130 and cathode 132 for a time period of about twenty-four hours. Finally, step 66 may involve supplying a current of 100 mA to anode 130 and cathode 132 for a time period of about twenty-four hours.

Referring to FIGS. 4 and 5, electrochemical cell 100 may include an electrolytic solution 170, an anode 130, and a cathode 132. Electrolytic solution 170 may comprise a metallic salt having a first metal that substantially absorbs deuterium when reduced to an atomic state, and a supporting electrolyte, each dissolved in heavy water. As an example, the metallic salt may be selected from the group of transition metals, such as palladium. In one embodiment, where the deuterium atoms bind to one another to create deuterium gas, the reduced metal 172, such as palladium, absorbs deuterium 174. In another embodiment, as shown in FIG. 5, gaseous deuterium atoms collect on the surface of cathode 132 and enter into the lattice of metal 172 when in a reduced state. In one implementation, electrolytic solution 170 comprises 20-25 mL solution of 0.03 M palladium chloride and 0.3 M lithium chloride in deuterated water.

Cathode 132 may be partially immersed in electrolytic solution 170. Cathode 132 may comprise a second metal that does not substantially absorb deuterium 174 and is generally stable in electrolytic solution 170 when cathode 132 is polarized. For example, cathode 132 may be comprised of Au, Ag, Pt, as well as their alloys. In some embodiments, cathode 132 may comprise a second metal that does absorb deuterium 174 and is generally stable in electrolytic solution 170 when cathode 132 is polarized. As an example, cathode 132 may be comprised of Ni or its alloys. Cathode 132 may be formed into various shapes, such as a wire, rod, screen, or foil. In some embodiments, cathode 132 may be shaped as a wire having a diameter of 0.25 mm and a length of 2.5 cm. Anode 130 may also be partially immersed in electrolytic solution 170 and may be stable in electrolytic solution 170 when anode 130 is polarized. Anode 130 may be manufactured from any electri-50 cally conductive material which is stable in electrolytic solution 170, such as Pt, as well as their alloys. The term "stable" with reference to anode 130 and cathode 132 means that the materials employed in the construction of anode 130 and cathode 132 do not substantially corrode when they are polarized and generally do not react with the electrolyte or products of electrolysis. Anode 130 may be formed into various shapes, such as a wire, rod, screen, or foil. As an example, anode 130 may be shaped as a wire having a diameter of 0.25 mm and a length of 30 cm.

FIG. 4 illustrates a front perspective view of an embodiment of a system 100 for generating particles using an external magnetic field. System 100 may include an electrochemical cell 110, power supply 140, and magnets 160. Cell 110 may include a body portion 120 and a top portion 122. Cell 110 may be rectangular, square, cylindrical, cubical, or various other shapes as recognized in the art. Cell 110, an example of which is commercially available from Ridout

Plastics, model AMAC, part number 752, may be comprised of various non-metallic materials that do not react with the electrolyte, such as butyrate. Body portion 120 may be configured to contain an electrolytic solution 170 (see FIG. 5). As an example, body portion 120 may be cubic in shape and may be comprised of a non-conductive material, such as plastic. Top portion 122 may be configured to cover body portion 120. Top portion 120 may be comprised of a non-conductive material, such as plastic. Top portion 122 may contain an opening 124 therein where an anode 130 may be passed therethrough, and also an opening 126 where a cathode 132 may be passed therethrough. Top portion 122 may also contain an opening 128 for venting purposes.

Anode 130 may comprise a wire mounted on a support 150 and may be partially immersed in electrolytic solution 170 15 (see FIG. 5). Support 150 may be comprised of a chemically inert material, such as polyethylene. Cathode 132 may be shaped as a single wire (as shown in FIG. 7A), a screen (as shown in FIG. 7B), or a foil (as shown in FIG. 7C). One end 131 of anode 130 may be connected to power supply 140. One 20 end 133 of cathode 132 may be connected to power supply 140. Power supply 140 may be a potentiostat/galvanostat, an example of which is commercially available from Princeton Applied Research, model 363. The other end 135 of anode 130 may be coupled to a support 150 (see FIG. 5), which may 25 be secured to body portion 120. Cathode 132 may be coupled to a particle detector 152 that may be attached to body portion 120. Both particle detector 152 and cathode 132 may be mounted to body portion 120. In one embodiment, particle detector 152 may be contiguous with cathode 132. In another 30 embodiment, detector 152 may be in proximity to cathode 132, such that particles emitted from cathode 132 may contact particle detector 152. For example, particle detector 152 may be positioned adjacent to cathode 132. As another example, particle detector 152 may be positioned between cathode 132 35 and body portion 120. Particle detector 152 may be used to detect the occurrence of particles.

Particle detector 152 may be comprised of a non-metallic material. In one implementation, particle detector 152 may be comprised of CR-39 material. CR-39 is a thermoset resin that 40 is chemically resistant to the electrolyte and to electromagnetic noise. CR-39 may be commercially obtained from Landauer. Particle detector 152 may comprise various shapes. As an example, particle detector 152 may be rectangular in shape with dimensions of 1 cm×2 cm×1 mm. When traversing a 45 plastic material such as CR-39, particles create along their ionization track a region that is more sensitive to chemical etching than the rest of the material. After treatment with an etching agent, tracks remain as holes or pits that may be seen with the aid of an optical microscope. The size, depth of 50 penetration, and shape of the tracks provides information about the mass, charge, energy, and direction of motion of particles generated by method 10. Neutral particles, like neutrons, will produce knock-ons, or charged particles resulting from the collision with the neutron that will leave ionization 55 tracks, or, with sufficient energy (e.g. >12 MeV) cause ¹²C present in the CR-39 resin to fission into 3 charged α particles that will leave ionization tracks.

Magnets 160 and 162 may be positioned adjacent to body portion 120 such that a magnetic field is created within electrochemical cell 100 between anode 130 and cathode 132 and though electrolytic solution 170. In some embodiments, the magnetic field created between magnets 160 and 162 may be sufficient to hold magnets 160 and 162 in position adjacent to body portion 120. In other embodiments, magnets 160 and 65 162 may be attached to body portion 120. Magnet 160 may be positioned adjacent to the surface of body portion 120 that

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contacts support 150. Magnet 162 may be positioned adjacent to the surface of body portion 120 that contacts detector 152. Magnets 160 and 162 may be comprised of various magnetic materials, such as NeFeB. As an example, the dimensions of magnets 160 and 162 may be 1 in×1 in×0.25 in. Magnets 160 and 162 may be commercially obtained from Dura Magnetics, part number NS-10010025. As an example, the external magnetic field created by magnets 160 and 162 may have a magnetic flux between about 1800 and 2200 Gauss. Magnets 160 and 162 may be permanent magnets or may be electromagnets.

FIG. 5 illustrates a cross-section view of a cell 110 during a co-deposition process. As shown, cell 110 is connected to power supply 140 and includes electrolytic solution 170 therein. Electrolytic solution 170 may comprise a soluble metallic salt (not shown) having a first metal, such as palladium, and a supporting electrolyte (not shown), wherein the palladium and chlorine are combined to form a palladium chloride complex anion, PdCl₄-. The palladium chloride complex anion may be dissolved in heavy water (D₂O) (not shown), with the palladium absorbing deuterium 174 when in a reduced state. The supporting electrolyte may include an ionizable salt to increase solution conductivity. Examples of ionizable salts may include: alkali metal chlorides, nitrates, and perchlorates. In one embodiment, electrolytic solution 170 may be comprised of a metallic salt such as 0.05 M PdCl₂ and a salt such as 0.3 M LiCl dissolved in 99.9 percent pure heavy water. During the co-deposition process, metal 172 infused with deuterium 174 may be deposited on cathode 132, while oxygen 176 accumulates around anode 130.

FIG. 6 illustrates a cross-section view of an embodiment of a system 200 for generating particles using an external electric field. System 200 may include an electrochemical cell 210, power supply 240, and external electrodes 260 and 262. Cell 210 may include a body portion 220 and a top portion 222. Top portion may contain an opening 224 (not shown) therein where an anode 230 may be passed there through, and also an opening 226 (not shown) where a cathode 232 may be passed there through. Top portion 222 may also contain an opening 228 (not shown) for venting purposes. Cell 210 may be rectangular, square, cylindrical, or various other shapes as recognized in the art. Cell 210 may be comprised of various non-metallic materials, such as butyrate. Anode 230 and cathode 232 may be connected to power supply 240. Power supply 240 may be a potentiostat or a galvanostat. Anode 230 is attached to a support 250. Cathode 232 may be coupled to a particle detector 254 that is attached to a support 256. Particle detector 254 may be comprised of a non-conductive material. In one implementation, particle detector 254 is comprised of CR-39 material.

Electrodes 260 and 262 may be positioned adjacent to body portion 220 such that an electric field may be created between anode 230 and cathode 232. In some embodiments, electrodes 260 and 262 may be secured to body portion 220 by an adhesive. Electrodes 260 and 262 are positioned adjacent to the surface of body portion 220 perpendicular to anode 230 and cathode 232. Electrodes 260 and 262 may be comprised of various conductive materials as recognized by one with ordinary skill in the art, such as copper. As an example, electrodes 260 and 262 may be less than one inch in diameter. Electrode 260 may be connected to a regulated high voltage source 264 via wire 266, whereas electrode 262 may be connected to regulated high voltage source 264 via wire 268. Wires 266 and 268 may comprise any suitable electrical wire as recognized by one with ordinary skill in the art. An example of a voltage source 264 that may be utilized with system 200 is voltage source model 4330, which may be

commercially obtained from EMCO. Voltage source 264 may be used to apply $6000 \mathrm{V}$ DC (with about 6% AC component) across electrodes 260 and 262.

Electrochemical cell 210 includes an electrolytic solution 270. Electrolytic solution 270 may comprise a metallic salt 5 having a first metal that substantially absorbs deuterium when in a reduced state (not shown), and a supporting electrolyte (not shown), each dissolved in heavy water (not shown). As an example, the metallic salt may be selected from the group of transition metals, such as palladium. In one embodiment, where the deuterium atoms bind to one another to create deuterium gas, the reduced deuterium absorbing metal 272, such as palladium, absorbs deuterium 274. In another embodiment, deuterium atoms collect on the surface of cathode 232 and enter into the lattice of deuterium absorbing metal 272 when in a reduced state. In one implementation, electrolytic solution 270 comprises 20-25 mL solution of 0.03 M palladium chloride and 0.3 M lithium chloride in deuterated water.

Referring to FIGS. 7A-7C, FIG. 7A shows a front view of 20 one side of an embodiment of system 100, illustrating an embodiment of the cathode 132. As shown, cathode 132 is attached to detector 152. In this implementation, cathode 132consists of a wire 134. As an example of a commercially available wire 134, may be obtained from Aldrich, Au wire 25 part number 326534 or Pt wire part number 349402. The cathode may be 0.25 mm in diameter, and be 3 cm in length. FIG. 7B illustrates a front view of one side of an embodiment of system 100, illustrating another embodiment of cathode 132. As shown, cathode 132 is attached to detector 152. In this 30 implementation, cathode 132 is formed as a screen 138. Screen 138 may serve to increase the surface area for particle emission. Screen 138 may be comprised of various metallic materials, such as Ni, Cu, Ag, and Au. As an example, a screen 138 commercially available from Delker, part number 3 Ni 35 5-077, is comprised of nickel, is 3 cm in size, has a thickness of 0.08 mm, and has eyelet dimensions of 1.5 mm×2.0 mm. FIG. 7C illustrates a front view of one side of an embodiment of system 100, illustrating another embodiment of cathode 132. As shown, cathode 132 is attached to detector 152. In this 40 implementation, cathode 132 is formed as a foil 139. Foil 139 may serve to increase the surface area for particle emission. Foil 139 may be comprised of various metallic materials, such as Ni, Cu, Ag, and Au. As an example, a foil 139 commercially available from Aldrich, part number 349267, is 2.5 cm 45 in size and has a thickness of 0.025 mm.

In the absence of an external electric/magnetic field, Scanning Electron Microscope (SEM) analysis of electrodes prepared by Pd/D co-deposition exhibit highly expanded surfaces consisting of small spherical nodules to form a 50 cauliflower-like morphology. Cyclic voltammetry and galvanostatic pulsing experiments indicate that, by using the co-deposition technique, a high degree of deuterium loading (with an atomic ratio D/Pd>1) is obtained within seconds. These experiments also indicate the existence of a $\rm D_2^+$ species within the Pd lattice. Because an ever expanding electrode surface is created, non-steady state conditions are assured, the cell geometry is simplified because there is no longer a need for a uniform current distribution on the cathode, and long charging times to achieve high deuterium loadings are eliminated.

Using the Pd/D co-deposition process, radiation emission and tritium production were documented. The results indicated that the reactions were nuclear in origin and that they occurred in the subsurface. To enhance these surface effects, 65 experiments were conducted in the presence of either an external electric or magnetic field. SEM analysis showed that

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when a polarized Au/Pd/D electrode was exposed to an external electric field, significant morphological changes were observed. These changes ranged from re-orientation and/or separation of weakly connected globules, through forms exhibiting molten-like features. EDX analysis of these features showed the presence of additional elements (in an electric field Al, Mg, Ca, Si, and Zn; in a magnetic field Fe, Cr, Ni, and Zn) that could not be extracted from cell components and deposited on discrete sites.

To verify that the new elements observed on the cathodes were nuclear in origin, the Pd/D co-deposition was done in the presence of a CR-39 detector. CR-39 is a polyallydiglycol carbonate polymer that is widely used as a solid state nuclear track dosimeter chip. When traversing a plastic material such as CR-39, charged particles create along their ionization track a region that is more sensitive to chemical etching than the rest of the bulk. After treatment with an etching agent, tracks remain as holes or pits and their size and shape can be measured

It should be noted that, in the area of modern dosimetry, CR-39 dosimeter chips are the most efficient detectors for the detection of light particles (alphas or protons). Experiments were conducted in which either a Ni screen or Au/Ag/Pt wire was wrapped around a CR-39 chip and was then used as the substrate for the Pd/D co-deposition. After the Pd was completely plated out, the cell was exposed to either an external electric or magnetic field. The experiment was terminated after two days and the CR-39 chip was etched using standard protocols (6.5 N NaOH at 70° C. for 6-7 hrs). After etching, the chip was examined under a microscope.

The Pd/D co-deposition generated pits in CR-39 have the same properties as those created by nuclear particles as shown in FIGS. 8A and 8B. FIGS. 8A and 8B are microphotographs 300 and 400, respectively, of tracks in CR-39 due to an alpha source. When the microscope optics are focused on the surface of the detector, as shown in FIG. 8A, it can be seen that the tracks 310 are symmetrical in shape and dark in color. When the microscope optics are focused inside the pits 410, as shown in FIG. 8B, bright spots 420 are observed. Tracks have a conical shape. The bright spot 420 is caused by the bottom of the track acting like a lens when the detector is backlit. The dark, symmetrical shapes with bright spots at their centers are diagnostic of nuclear generated tracks.

FIGS. 8C and 8D show microphotographs 500 and 600, respectively, of Pd/D co-deposition generated tracks 510 and 610 obtained by focusing the microscope optics on the surface and the bottom of the pits, respectively. It can be seen that the Pd/D co-deposition generated tracks are dark and symmetrical in shape, with bright spots 520 and 620, respectively, inside them.

FIGS. 9A and 9B show images taken of the CR-39 detector after a Pd/D co-deposition experiment in a magnetic field. FIG. 9A illustrates a magnified image 700 of a CR-39 taken after a Pd/D co-deposition experiment in a magnetic field in accordance with an embodiment of the system and method for generating particles. FIG. 9B illustrates a further magnified image of image 700.

The electrode substrate used to create these images is a 0.25 mm diameter Ag wire. Visible inspection of the CR-39 chip showed a cloudy area where the electrode substrate was in close proximity to the CR-39 detector. The cloudy area 710 shown in FIG. 9A is approximately 0.5 mm wide and 4.6 mm long. The fact that the cloudy area was only observed where the detector was in close proximity to the cathode indicates that the cathode has caused the cloudiness. The 500× magnification of the center of the cloudy area shown in FIG. 9B illustrates the presence of numerous overlapping tracks 720,

both large and small. The number of tracks is far more than are observed in laser fusion experiments (typically DD or DT).

FIGS. 10A and 10B show a side-by-side comparison of features observed when the detector is exposed to depleted U and a detector that has undergone exposure to a Pd/D codeposition experiment in the presence of an external electric field. FIG. 10A illustrates a magnified image 800 of a CR-39 detector exposed to depleted uranium. FIG. 10B illustrates a magnified image 900 of a CR-39 detector exposed to a Pd/D codeposition experiment performed on a Au wire in the presence of a 6000V external electric field in accordance with the disclosed subject matter. Since the features look the same, and since depleted Uranium is giving off alphas, it stands to reason that the features observed for the codeposition experiment are also due to high energy particles. These particles can be either alphas, protons, or neutrons.

It should be noted that in the absence of an external electric/magnetic field, when Ni screen is used as the cathode, no tracks are observed on the CR-39 chip, as shown in FIG. 11. FIG. 11 illustrates an image 1000 of a CR-39 detector indicating X-ray emission, in accordance with an embodiment of the system and method for generating particles. Instead of tracks, the impression of the electrode substrate is observed in the CR-39 detector which has been caused by the emission of soft X-rays from the cathode.

The size of the tracks is proportional to the energy of the particle that created the track. It has been observed that the energy of the particles created in these experiments can be controlled by the electrode substrate. When the Pd/D codeposition reaction is done on a light Z material such as Ni, the particles are small and homogeneous in size, as shown in image 1100 shown in FIG. 12A. However, when the reaction is done on a higher Z material, such as Ag, Au, or Pt, both large and small particles are observed, as shown in FIGS. 9A, 9B, 10B, 12A, and image 1200 shown in FIG. 12B.

FIG. 13A shows an SEM image 1300 of the Pd deposit on Au foil that has been exposed to a magnetic field. The Lorentz lines of the magnetic field have caused the Pd micro-globules to form star-like features. FIGS. 13B-13D show images 1400, 1500, and 1600, respectively, taken of a CR-39 detector after a Pd/D co-deposition experiment in a magnetic field using a Ag wire cathode. FIG. 13B shows that the tracks coincide with the Pd deposit indicating that the Pd deposit is the source of the tracks. FIGS. 13C and 13D show magnified images of the tracks. The tracks vary in size indicating that particles of 45 different types and energies are being produced.

Specific Example

Materials

Palladium chloride (99%, Aldrich), lithium chloride (analytical grade, Mallinckrodt), deuterated water (99.9% D, Aldrich), 0.25 mm diameter gold wire (99.9%, Aldrich), 0.5 mm diameter silver wire (99.9% Aldrich), 0.25 mm diameter platinum wire (99.9%, Aldrich), nickel screen (Delker, 0.35 55 mm thick and eyelet dimensions of 3 mm×1.9 mm). Cell Design

Cell design as shown in FIGS. **4-6**. Charging Procedure

Typically 20-25 mL solution of 0.03 M palladium chloride 60 and 0.3 M lithium chloride in deuterated water is added to the cell. Palladium is then plated out onto the cathode substrate using a charging profile of 100 μA for 24 h, followed by 200 μA for 48 h followed by 500 μA until the palladium has been plated out. This charging profile assures good adherence of 65 the palladium on the electrode substrate. Once the palladium has been plated out of solution, the external electric or mag-

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netic fields are applied. In the external electric field configuration as shown in FIG. 6, copper electrodes (~1 inch in diameter) are taped to the outside of the cell wall. A regulated high voltage source (EMCO model 4330) is used to apply 6000 V DC (and has a ~6% AC component) across these copper electrodes. In the magnetic field configuration as shown in FIGS. 4 and 5, the attractive forces between the 1 in×1 in×0.25 in permanent NdFeB magnets (available from Dura Magnetics) hold them in place on either side of the cell, as shown in FIGS. 4 and 5. The strength of the magnetic field is on the order of 2000 Gauss. After the palladium has been electrochemically plated out and the external field has been applied, the cathodic current is increased to 1 mA for 2 h, 2 mA for 6 h, 5 mA for 24 h, 10 mA for 24 h, 25 mA for 24 h, 50 mA for 24 h, 75 mA for 24 h, and 100 mA for 24 h. Summary of Results

With a Ni screen cathode and no external field, there is X-ray emission (see FIG. 11). There are charged particles seen (alphas and protons) when an external electric or magnetic field is applied. For cathodes made of higher Z materials (Ag, Au, Pt), charged particles are obtained in the absence of an external field. Tracks are observed on the back of the CR-39 which is indicative of neutron generation. The neutrons produced can have various energy levels. Besides the emission of alphas, protons, soft X-rays, and neutrons, the cells also produce tritium, gammas, and betas.

A summary of some necessary conditions to obtain pits are contained in Table 1 shown below. The column labeled "Experiment" indicates the type of cathode used, while the "Field" column indicates whether an electric or magnetic field was used. Unless otherwise indicated, Pd/D co-deposition was performed using LiCl and D₂O.

TABLE 1

| Experiment | Field | Result |
|---|---------------|--|
| Ni screen | None | No pits, see impression of Ni |
| | | screen |
| Ni screen | E or B | Pits in patches |
| Ag wire | None, E, or B | High density of pits |
| Au or Pt wire | E or B | High density of pits |
| Ag, KCI | E or B | High density of pits |
| Ag, H_2O | E or B | Pits, less dense than D ₂ O |
| Pd wire, no co-dep | E or B | Pits in patches |
| CuCl ₂ in place of PdCl ₂ | None, E, or B | No pits |

Additionally, Table 2 shown below represents a summary of experiments performed to determine if the CR-39 pits were due to contamination or electrolysis.

TABLE 2

| Experiment | Result |
|---|---------|
| Place PdCl ₂ powder on surface of CR-39 | No pits |
| Immerse CR-39 in PdCl ₂ —LiCl—D ₂ O | No pits |
| Wrap cathode substrates around CR-39 | No pits |
| Electrolysis using Ni screen and LiCl—D ₂ O | No pits |

Many modifications and variations of the system and method for generating particles are possible in light of the above description. Therefore, within the scope of the appended claims, the system and method for generating particles may be practiced otherwise than as specifically described. Further, the scope of the claims is not limited to the embodiments and implementations disclosed herein, but extends to other embodiments and implementations as may be contemplated by those with ordinary skill in the art.

We claim:

1. A method comprising the steps of:

supplying more than one current levels, each current level not exceeding about $500~\mu\mathrm{A}$, to the anode and the cathode of an electrochemical cell according to a first charging profile, wherein the electrochemical cell comprises: a body portion,

an electrolytic solution, contained within the body portion, comprising a metallic salt, comprising palladium, and a supporting electrolyte, each dissolved in heavy water.

a cathode immersed in the electrolytic solution and vertically disposed adjacent to a first side of the body portion, the cathode comprising a metal that does not substantially absorb deuterium and is stable in the lectrolytic solution when the cathode is polarized, and

an anode immersed in the electrolytic solution apart from the cathode and vertically disposed adjacent to a second side of the body portion, the second side ²⁰ located opposite the first side, wherein the anode is stable in the electrolytic solution when the anode is polarized; and

maintaining each of the supplied more than one current levels at a generally constant level during the first charging profile such that deposition of palladium on the cathode occurs in the presence of evolving deuterium gas during electrolysis of the electrolytic solution.

2. The method of claim 1, wherein the metal is selected from the group of metals consisting of nickel, gold, silver, and ³⁰ platinum, and their alloys.

3. The method of claim 1, wherein the cathode is formed as a foil.

4. The method of claim 1, wherein the step of supplying more than one current levels, each current level not exceeding about 500 μ A, to the anode and the cathode of an electrochemical cell according to a first charging profile includes the

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steps of supplying a current of about 100 μA to the anode and the cathode for a time period of about twenty-four hours, supplying a current of about 200 μA to the anode and the cathode for a time period of about forty-eight hours and supplying a current of about 500 μA to the anode and the cathode until deposition of metallic ions on the cathode terminates.

5. The method of claim **1**, wherein the metal comprises nickel and the cathode is formed as a screen.

6. The method of claim 5 further comprising the steps of: exposing the electrochemical cell to an external magnetic field after the termination of the deposition of the palladium on the cathode; and

supplying current to the anode and the cathode according to a second charging profile during the exposure of the electrochemical cell to the external magnetic field.

7. The method of claim 6, wherein the step of supplying current to the anode and the cathode according to a second charging profile includes the steps of:

supplying a current of about 1 mA to the anode and the cathode for a time period of about two hours;

supplying a current of about 2 mA to the anode and the cathode for a time period of about six hours;

supplying a current of about 5 mA to the anode and the cathode for a time period of about twenty-four hours;

supplying a current of about 10 mA to the anode and the cathode for a time period of about twenty-four hours;

supplying a current of about 25 mA to the anode and the cathode for a time period of about twenty-four hours;

supplying a current of about 50 mA to the anode and the cathode for a time period of about twenty-four hours;

supplying a current of about 75 mA to the anode and the cathode for a time period of about twenty-four hours; and

supplying a current of about 100 mA to the anode and the cathode for a time period of about twenty-four hours.

* * * * *